# Solute Dispersion by Electroosmotic Flow in Nonuniform Microfluidic Channels

M.T. Blom<sup>1</sup>, E. F. Hasselbrink<sup>2</sup>, H. Wensink<sup>1</sup>, A. van den Berg<sup>1</sup>
<sup>1</sup>University of Twente, MESA+ Research Institute, Enschede, The Netherlands
<sup>2</sup>Sandia National Laboratories, PO Box 969, MS 9951, Livermore, CA 94550

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## Introduction

Dispersion is a phenomenon that determines the resolution of several types of liquid phase chromatography, and is an important component of overall transport through electrokinetic flow systems. The severe dispersion of solute as it travels through a U-turn, for example, has attracted recent attention for this reason [1]. In "ideal" electroosmotic flow through uniform, straight channels (in the limit of thin double layers), solute dispersion is simply due to axial diffusion. However, in straight microfabricated channels, channel nonuniformities may arise due to surface roughness (e.g., due to etching or powderblasting fabrication methods [2]), or imperfections (e.g., etch pits, waviness due to poor resist adhesion, or imperfect bonding of channel lids). Other nonuniformities may be intentional, e.g., engineered post arrays for electrochromatography. In this work, we measure dispersion in several types of nonuniform channels, and report their geometric Taylor-Aris dispersion coefficients  $\alpha_0$ . The dispersion coefficient relates the effective diffusion coefficient  $D_{eff} = D_{12}(1 + \alpha_0 Pe^2)$ , to the binary diffusion coefficient,  $D_{12}$  as a function of the Peclet number [3,4].

#### Measurements

Measurements are performed in glass channels using a custom-built fluorescence imaging apparatus. The two types of perturbations studied are (a) well-defined perturbations (square-wave and sawtooth) of various wavelengths and amplitudes (Fig. 1), and (b) fine-scale random roughness introduced by a powderblasting channel fabrication method (Fig. 2). Samples of Rhodamine-110 dye (in a 50:50 solution of 20mM phosphate buffer and acetonitrile) are injected into several parallel channels of different waviness, as shown in Fig. 3. As the samples move through the channels, they assume a Gaussian profile of width  $\sigma^2 = 2D_{eff}t + \sigma_o^2$ , where t is time and  $\sigma_o$  is the initial plug width. Gaussian fits to profiles in a single channel (Fig. 4) give values of  $\sigma^2$  at various times; plotting this versus time gives a straight line of slope  $2D_{eff}$ .

#### **Results**

Measurements of  $D_{12}$  (with no flow, Pe=0) were repeatable to within 2%. Performing the experiment at several Peclet numbers (varied by increasing the applied electric field), provides  $D_{eff}$  versus  $Pe^2$ , which gives the dispersion coefficient  $\alpha_o$  for a given geometry. Results for several geometries are shown in Fig. 5. The largest dispersion coefficient is  $1.6*10^{-3}$  (for the large perturbation channels). Extending these results to large molecules of low diffusivity, it is possible (at, say, Pe=1000) to reach effective diffusivities which are more than 2.5 times the binary diffusion coefficient.

## References

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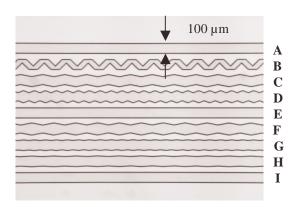


Fig. 1: Picture of the sawtooth-shaped channels (depth 13  $\mu$ m) that were studied. Channels have perturbations of various amplitudes (0, 3 or 10  $\mu$ m) and wavelengths (100 or 200  $\mu$ m).

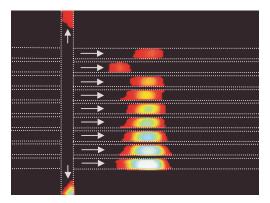


Fig. 3: Injection part of the chip shown in Fig. 1 showing injected plugs of fluorescent dye used for characterization of the dispersion

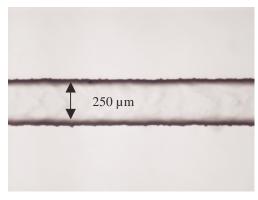


Fig. 2: Picture of a microfluidic channel fabricated using powderblasting with 9  $\mu$ m particles giving a channel roughness of approx. 1  $\mu$ m.

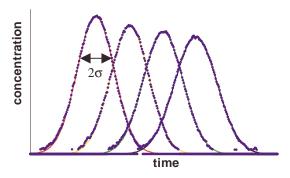


Fig. 4: Measured concentration profiles at various times fitted by Gaussian curves giving the variation of the plug variances with time.

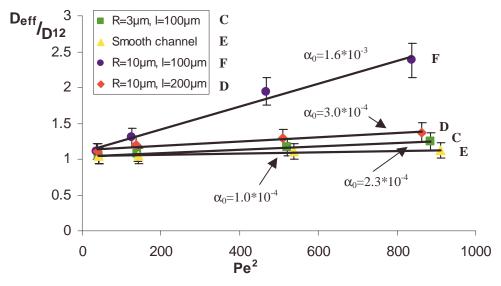


Fig. 5: Graph showing the measured ratio of the effective diffusivity  $D_{eff}$  over the binary diffusion coefficient  $D_{12}$  at various  $Pe^2$  numbers for channels C,D,E,F from Fig.1. It is clear from this graph that the dispersion, given by the curve slopes, is higher for rougher channels. The effect of increasing perturbation amplitude and decreasing wavelength appears to be more than proportional.